# FEB - FRESENIUS ENVIRONMENTAL BULLETIN

Founded jointly by F. Korte and F. Coulston Production by PSP - Vimy Str. 1e, 85354 Freising, Germany in cooperation with PRT-Parlar Research & Technology Vimy Str 1e, 85354 Freising

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Printed in Germany-ISSN 1018-4619



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# **CONTENTS**

# **ORIGINAL PAPERS**

FUMIGANT TOXICITY OF FIVE PLANT ESSENTIAL OILS AGAINST CITRUS MEALYBUG, <i>PLANOCOCCUS CITRI</i> RISSO (HEMIPTERA: PSEUDOCOCCIDAE) <b>Tugba Erdemir, Fedai Erler</b>	3231
AN ASSESSMENT OF SURFACE SOIL MOISTURE BASED ON <i>IN SITU</i> OBSERVATIONS AND LANDSAT 8 REMOTE SENSING DATA Chunya Ma, Jinglei Wang, Zhen Chen, Zhifang Chen, ZhanDong Liu, Xiuqiao Huang	3236
TRANSPORTATION OF INFLUENZA VIRUS AROUND BUILDINGS IN NATURAL WIND FIELD Wei Liu, Xue-Yi You	3245
<i>TRICHODERMA</i> INOCULUM AND ELEVATED AMIBIENT CARBON DIOXIDE ENHANCED PHYTOEXTRACTION OF Zn-CONTAMINATED SOIL BY <i>LOLIUM MUTIFLORUM</i> <b>Ningning Song, Haiyun Li, Qi Guo, Jun Liu, Fangli Wang, Kairong Wang</b>	3252
CHANGES IN HEAVY METAL FLUXES IN CONTAMINATED SOIL INOCULATED WITH <i>BURKHOLDERIA</i> SP. AND PENICILLUM SP. MEASURED BY DGT Jun Liu, Shaojing Li, Haiyun Li, Fangli Wang, Kairong Wang, Ningning Song	3259
RESPONSES OF SOIL NEMATODE COMMUNITIES TO HERBICIDE TOLERANT SOYBEAN Zhiguo Yang, Lili Wang, Dianlin Yang, Gang Li, Weiming Xiu, Hongmei Liu, Xin Lai, Hui Wang, Hong Chang, Jianning Zhao	3266
SOLAR OXIDATION OF AN INTEGRATED WOOD INDUSTRY WASTEWATER Neval Baycan	3276
PREPARATION OF Cu-LDHS BY REUTILIZING Cu FROM ELETROPLATING WASTEWATER AND ITS APPLICATION TO IODIDE REMOVAL Xiaping Zhu, Yuan Zhou, Jie Zheng	3284
SEQUENCING AND ANALYSIS OF NORMALIZED FULL-LENGTH CDNA LIBRARY FROM HYPODERMA SINENSE PLESKE LARVAE Ping Fan, Ming Kang, Ruiqiang Zhang	3290
THE INFLUENCE OF FOLIAR APPLICATION OF SILICON ON INSECT DAMAGE AND DISEASE OCCURRENCE IN FIELD TRIALS Joanna Zamojska, Jakub Danielewicz, Ewa Jajor, Radoslaw Wilk, Joanna Horoszkiewicz-Janka, Daria Dworzanska, Pawel Wegorek, Marek Korbas, Pankracy Bubniewicz, Wieslaw Ciecierski, Jan Narkiewicz-Jodko	3300
DRIVING MECHANISMS AND PEAK LEVELS OF CO₂ EMISSIONS IN CHINA: EVIDENCE FROM A SIMULTANEOUS EQUATION MODEL Feng Dong, Xinqi Gao, Haimiao Yu, Ruyin Long	3306
THE EFFECT OF SHORT-TERM EXPOSURE TO LOW pH/ALUMINUM ON THE ION REGULATION, RELATED ATPase ACTIVITIES AND HAEMATOLOGICAL PARAMETERS OF JUVENILE COMMON CARP Hong-Jie Sun, Yu Zhang, Emmanuel Ndayambaje, Wen-Qi Dong, Hong-Jun Lin, Jian-Rong Chen, Hua-Chang Hong	3318
COMPARISON OF REAL-TIME PCR, RT-PCR AND MOLECULAR HYBRIDIZATION TECHNIQUES FOR THE DIAGNOSIS OF GYSVD-1 ( <i>GRAPEVINE YELLOW SPECKLE VIROID-1</i> ) IN GRAPEVINES Ismail Can Paylan, Ayse Candar, Serkan Onder, Nihan Gunes, Mustafa Gumus, Semih Erkan	3326
ECONOMICAL ASPECTS OF CONSERVATION AGRICULTURE (ZERO TILLAGE-DIRECT SEEDING) SYSTEM IN TURKEY Mustafa Kan, Fevzi Partigoc, Irfan Gultekin, Rifat Zafer Arisoy, Yasin Kaya, Serpil Gultekin, Mehmet Sahin, Seydi Aydogan, Fatih Ozdemir, Alper Taner	3332
LEAVES POWDER OF SYZGIUM CUMINI AS AN ADSORBENT FOR REMOVAL OF CONGO RED DYE FROM AQUEOUS SOLUTION Muhammad Imran Khan, Shagufta Zafar, Muhammad Farooq Azhar, Abdul Rehman Buzdar, Warda Hassan, Abida Aziz, Majeda Khraisheh	3342
<i>in vitro</i> effects of new generation bisoxadiazole substituted sulfonamide derivatives on human serum paraoxonase1 (pon1) Mustafa Oguzhan Kaya, Ozcan Gulec, Mustafa Arslan	3351



DETERMINATION OF SOIL LOSSES USING RUSLE MODEL AND GEOGRAPHICAL INFORMATION SYSTEMS (GIS) IN A SELECTED AREA IN MEDITERRANEAN REGION OF TURKEY <b>Ozan Artun, Yakup Kenan Koca</b>	3359
OCCURENCE OF OCHRATOXIN A IN BOTANICAL PRODUCTS COMMERCIALIZED IN TURKEY Hakan Ozden, Sibel Ozden	3367
EFFECTS OF THE EXTRACT FROM DIFFERENT PLANT PARTS OF <i>FERULA COMMUNIS</i> SPP. <i>COMMUNIS</i> ON THE SEED GERMINATION AND SEEDLING GROWTH OF BARLEY AND CUCUMBER <b>Bengu Turkyilmaz-Unal, Aylin Esiz-Dereboylu, Aykut Guvensen, Nedret Tort, Munir Ozturk</b>	3375
FLOCCULATION AND REMOVAL OF <i>MICROCYSTIN AERUGINOSA</i> CELLS BY NATURAL FLOCCULANT FROM POMEGRANATE PEEL Hongqiang Wang, Qingliang Wang, Ying Xiong, Eming Hu, Wenfa Tan, Lieyu Zhang	3382
LALA CLAM ( <i>ORBICULARIA ORBICULATA</i> ) SHELL AS AN ADSORBENT FOR ANIONIC AND CATIONIC DYES FROM AQUEOUS SOLUTION	3386
Azlan Kamari, Arwa Alseddig Ahmed Eljiedi, Endang W Laksono, Norlaili Abu Bakar	
UNCERTAINTY ANALYSIS OF HUMAN HEALTH RISK ASSESSMENT CAUSED BY LOW CONCENTRATION ARSENIC CONTAMINATION IN THE COAL CHEMICAL SITE	3399
Shihai Zhang, Linying Yao, Sa Xiao, Shasha Yang, Haibin He, Zihao Wang, Jianli Jia	
kriging risk model of dam failure based on hl-rf algorithm Xiao Fu, Chongshi Gu, Xueqin Zheng, Huaizhi Su, Xiangnan Qin	3409
LEVELS OF CADMIUM AND LEAD IN CANNED MEAT CONSUMED IN SAUDI ARABIA Muhammad Waqar Ashraf, Abdus Salam	3419
CHEMICAL PROPERTIES AND FERTILIZER VALUE OF TEN DIFFERENT ANAEROBIC DIGESTATES Magdalena Szymanska, Ewa Szara, Tomasz Sosulski, Wojciech Stepien, Krzysztof Pilarski, Agnieszka A Pilarska	3425
local sustainability: evaluating visitors' level of satisfaction in cumalikizik, turkey Ismail Bulent Gurbuz, Mike Manaros	3433
THE ABSORPTION CONDITION OF MERCURY IN MERCURY-CONTAMINATED SOILS BY OPUNTIA STRICTA Zhongchuang Liu, Li-ao Wang, Shimin Ding	3439
THE USE OF BIOINDICATORS FOR ASSESSING ATMOSPHERIC POLLUTION WITH PLATINUM METALS <b>Renata Komendova</b>	3444
SHORT-TERM RESPONSES OF SOIL CONE INDEX AND BIOPORE WITH DIFFERENT RATES OF STRAW INCORPORATION IN RICE – WHEAT CROPPING SYSTEM Eisa Belal, Ding Qishuo, He Ruiyin, Yinian Li, Khurram Yousaf, John Fielke	3452
EXOTIC MYCORRHIZAE SPECIES INOCULATED PLANT SPECIES GROUPS HAVE DIFFERS EFFECTS ON ROOT COLONIZATION AND SPORULATION Cagdas Akpinar, Ibrahim Ortas, Ahmet Demirbas	3462
CHARACTERIZATION AND PURIFICATION OF THE INTRACELLULAR PHYTASE FROM OCHROBACTRUM ANTHROPI Afet Arkut, Sadik Dincer, Hatice Aysun Mercimek Takci, Melis Sumengen Ozdenefe, Fikret Buyukkaya Kayis	3469
ASSESSMENT OF ON-CAMPUS NOISE LEVELS AT CUMHURIYET UNIVERSITY Fuat Ozyonar, Omur Gokkus, Hamdi Muratcobanoglu, Onder Gursoy	3476
EFFECTS OF SODIUM CHLORIDE ON PROKARYOTIC MICROBIAL COMMUNITY IN CHINESE TRADITIONAL FOOD PAOCAI Pingmei Yan, Zheng Chai, Xiaohui Chang, Hongping Qiao, Wenjing Zhao, Miaowen Cao	3482
SHALLOW GROUNDWATER UTILIZATION ROLE OF WHEAT BASED ON DIFFERENT SOIL AND DIFFERENT GROUNDWATER DEPTH Mei Zhu, Bazai Nazir Ahmed, Xueling Li, Mengnan Huang, Tahir Muhammad, Lei Ming	3495
EFFECTS OF DIFFERENT DRYING METHODS ON THE DETERMINATION OF NITROGEN IN SEDIMENT Xiansheng Liu, Cencen Yu, Guoxiang Wang, Yaqi Hu	3506
ANALYSIS OF LANDSCAPE PATTERNS AND CONNECTIVITY BETWEEN TREE CLUSTERS DERIVED FROM LIDAR DATA Serdar Selim, Nusret Demir	3512

FEB

VISUAL QUALITY ASSESSMENT OF ROADSIDE GREEN SPACES IN THE URBAN LANDSCAPE - A CASE STUDY OF BELGRADE CITY	3521
Nadezda Stojanovic, Nevena Vasiljevic, Boris Radic, Dejan Skocajic, Nevenka Galecic, Mirjana Tesic, Aleksandar Lisica	
ASSESSING ECOSYSTEM SERVICES OF BORNOVA'S GREEN INFRASTRUCTURE, IZMIR (TURKEY) Cigdem Coskun-Hepcan, Serif Hepcan	3530
EFFECT OF INTERSPECIFIC COMPETITION ON THE GROWTH OF ALIEN SPECIES SAGITTARIA GRAMINEA AND LOCAL RELATIVES Lihui Zhang, Yanwen Zhang, Jimin Zhao	3542
THE ORAL EXPOSURE HEALTH RISK ASSESSMENT OF A CITY IN CHINA BASED ON INTEGRATED APPROACH Yan Yang, Xin Wen, Liang Liu, Ningyi Yuan, Yunjiang Yu, Zhixiang Xing	3549
THE EFFECT OF BORON ON THE MORPHOLOGICAL AND PHYSIOLOGICAL RESPONSES OF SUNFLOWER SEEDLINGS (HELIANTHUS	3554
Ramazan Beyaz, Mehtap Gursoy, Murat Aycan, Mustafa Yildiz	
EFFECTS OF LANDSCAPE CHANGES ON ECOSYSTEM SERVICES: A CASE STUDY IN NANPING, NORTHERN FUJIAN PROVINCE,	3561
Xuncheng Fan, Jianbin Liu, Jianzhong Chen, Lili Zhao, Wei Hong, Tao Hong, Han Lin	
ISOLATION AND CHARACTERIZATION OF RHIZOSPHERIC BACTERIA FOR BIOCONTROL OF TOMATO BACTERIAL SPECK DISEASE	3571
H Nilufer Yildiz, H Handan Altinok, Murat Dikilitas, Tahsin Ay, Hale Gunacti	
GENOTYPE REACTION AND EFFECT OF THE SOWING TIME UNDER ARID ECOLOGICAL CONDITIONS IN SAFFLOWER (CARTHAMUS TINCTORIUS L.) Arzu Kose, Halil Hatinoglu, Husevin Arslan	3577
ANTIOXIDANT PROPERTIES OF THYMUS FLORAL WATER USING SQUARE WAVE ELECTROCHEMICAL METHODS AND RADICAL	3587
trapping Amir Yousefi, Mohammad Hadi Givianrad, Hessam Sepasi Tehrani	5507
COMPARISON OF SQUARE WAVE AND DPPH METHOD FOR DETERMINATION OF ANTIOXIDANT CAPACITY OF AJWAIN Zahra Khoramian, Mohammad Hadi Givianrad, Hessam Sepasi Tehrani	3592
A STUDY ON AIR POLLUTION FEATURECLASSIFICATION OF MAJOR CITIES IN THE MIDDLE REACHES OF THE YANGTZE RIVER Zhi-lin Hu, Pei-jiang Zhou, Feng Ye	3597
SOIL-ATMOSPHERE CO2, CH4 AND N2O FLUXES FROM A PEATLAND IN THE CONTINUOUS PERMAFROST ZONE, NORTHEAST	3606
Changchun Song, Yuqing Miao, Xianwei Wang, Henan Meng	
EVALUATING THE IMPACT OF GEOTHERMAL WATER ON GROWTH, LIPID ACCUMULATION AND FATTY ACID COMPOSITION BY SPIRULINA PLATENSIS Ova Irmak Sahin Arzu Akninar-Bayizit	3617
RELATIONSHIP RETWEEN SPECTRAL REFLECTANCE AND PLANT NUTRIENT ELEMENT.CHLOROPHYLL CONTENT IN LETTLICE	2624
(LACTUCA SATIVA L.) GROWING Sevda Altunbas, Gafur Gozukara, Namik Kemal Sonmez, Ahmet Safak Maltas, Mustafa Kaplan	3024
STUDIES ON THE OXIDATIVE ADSORPTION CAPABILITY OF Mg-Mn SPINELS AS SULFUR TRANSFER CATALYSTS <b>Tao Zhu, Xiu Jun Ji, Yu Dong Zhou, Hao Tian, Wei Wang, Rui Yu Jiang</b>	3633
ANALYSIS ON MECHANISM OF WATER-INDUCED LANDSLIDES AND MONITORING CONTROL SCHEME ESTABLISHMENT Qian Zhang,Yong Liu, Yinghua Tan, Jing Wang, Songsong Bai, Yaoxin Si	3639
LIFE HISTORY STRATEGIES IN TWO BRACHIONUS CALYCIFLORUS (ROTIFERA) EVOLVING SPECIES: RESPONSES TO TEMPERATURE CHANGE	3645
Qiu-Lei Xu, Jia-Nan Li, Xian-Ling Xiang, Hai-Xia Tan, Yi-Long Xi	
NOCARDIA SP. STRAIN SJJ-8-7 ISOLATED FROM A KARST CAVE IN SOUTHWESTERN CHINA PRECIPITATES CALCIUM CARBONATE	3654

Zi-Qi Liu, Jian-Jian Jiang, Qiu-Fang He, Kang-Ning Xiong, Rui-Yi Zhao, Xian-Fu Lv

Fresenius Environmental Bulletin

SPATIOTEMPORAL VARIABILITY IN HYDRO-METEOROLOGICAL TIME SERIES DATA USING NON-PARAMETRIC TESTS OVER HINDU KUSH, HIMALAYAN AND KARAKORAM RANGES IN PAKISTAN Moien Ahsan, Abdul Sattar Shakir, Fan Zhang, Sonia Zafar, Ghulam Nabi, Ijaz Ahmad	3666
CHARACTERIZATION OF BIOCHARS DERIVED FROM MAIZE STRAW AND CORN COB AND EFFECTS OF THEIR AMENDMENT ON MAIZE GROWTH AND LOESS SOIL PROPERTIES <b>Tawheed Mohammed Elheesin Shareef, Baowei Zhao, Mikalai Filonchyk</b>	3678
STUDY ON PREPARATION AND PERFORMANCE OF NANO-ZINC OXIDE Qingyun Ren, Songtao Wang	3687
EVALUATION OF ENVIRONMENT QUALITY IN GOAF WATER OF YUNGANG MINING AREA IN DATONG, SHANXI, CHINA Jun Li, Herong Gui, Huili Qiu, Leisheng Guan, Pengfei Ding	3692
STUDY ON GASIFICATION OF CORN STALK IN SUPERCRITICAL WATER Qing Xu, Wei Yang, Changming Ling	3701
EFFECT OF THREE <i>BACILLUS</i> SPP. ON TOBACCO WHITEFLY <i>BEMISIA TABACI</i> (GENNADIUS) (HOMOPTERA: ALEYRODIDAE) Osama W Al Arabiat, Salah-Edden A Araj, Kholoud M Alananbeh, Tawfiq M Al-Antary	3706
ANTI-BIOFILM, ANTIMICROBIAL AND CYTOTOXIC ACTIVITY OF ACHILLEA MILLEFOLIUM L. ESSENTIAL OIL ${f Ugur \ Tutar}$	3713
EFFECTS OF EM ( <i>EFFECTIVE MICROORGANISM</i> ) ORGANIC FERTILIZER APPLICATION ON THE SOIL ENVIRONMENT UNDER GREENHOUSE CONDITION Zhiyuan Lin, Zuzhi Chen, Xinyu Lu, Jiyu Li, Weiqi Yan, Chang Liu, Yankai Ruan, Shuang Liu, Fenglin Zhong, Maomao Hou	3721
GENETIC PARAMETERS AND PATH COEFFICIENT ANALYSIS IN CHICKPEA ( <i>CICER ARIENTINUM</i> L.) Aybegun Ton, Adem Emin Anlarsal	3728
BENEFICIAL AND POTENT EFFECT OF OLIVE LEAVES EXTRACT ON HYPERGLYCEMIC STATE, KIDNEY AND LIVER FUNCTION IN STZ- INDUCED TYPE 2 DIABETES MELLITUS Abd El-Moneim M R Afify, Hossam S El-Beltagi, Sayed A Fayed, Abeer E El-Ansary	3733
trace metals concentration of sea cucumber ( <i>actinophyga bannwarth</i> and <i>holothuria impatiens</i> ) from the red sea, gulf of aqaba <b>Tariq Al-Najjar, Mustafa Alshabi, Mohammad Wahsha, Ahmad Abu-Hilal</b>	3740
INFLUENCE OF THREE <i>BACILLUS</i> SPP. ON DIFFERENT PARAMETERS OF CAULIFLOWER PLANT GROWTH WHEN TESTED ON TOBACCO WHITEFLY <i>BEMISIA TABACI</i> (GENNADIUS) (HOMOPTERA: ALEYRODIDAE) Osama W Al Arabiat, Salah-Edden A Araj, Kholoud MAlananbeh, Tawfiq M Al-Antary*	3746
THE WATER QUALITY OF STREAMS FLOWING INTO SOUTH EASTERN BLACK SEA COASTS IN TERMS OF PHYSICO-CHEMICAL PROPERTIES TANJU Mutlu, Bulent Verep	3752
A CASE STUDY OF ENERGY BALANCE AND ENERGY ECONOMICS ANALYSIS OF IRRIGATED WHEAT PRODUCTION IN TURKEY <b>Okan Demir</b>	3759
EFFECTS OF VITAMIN D ON MATRIX METALLOPROTEINASE 9 AND APOPTOSIS IN EXPERIMENTAL DIABETIC RAT KIDNEY TISSUE Nevzat Gozel, Fatih Genc, Fethi Ahmet Ozdemir, Tuncay Kuloglu, Nalan Kaya, Mehmet Hanifi Yalcin, Sule Kavak-Genc, Suleyman Serdar Koca, Emir Donder	3766
ANALYSIS OF TARGETS TO BE REACHED WITH SUSTAINABLE PRODUCTION IN FOREST PRODUCTS AND INDUSTRY ENTERPRISES: THE CASE OF THE WESTERN BLACK SEA REGION <b>Tarik Gedik, Muhammet Cil</b>	3776
THE EFFECTS OF SALT STRESS, SNP, ABA, IAA AND GA APPLICATIONS ON ANTIOXIDANT ENZYME ACTIVITIES IN HELIANTHUS	3783

**Oguz Ayhan Kirecci** 

ANNUUS L.

EVALUATING SPECTRAL REFLECTANCE VEGETATION INDEXES TO PREDICT CHLOROPHYLL CONTENT IN SORGHUM (SORGHUM 3789 BICOLOR) PLANTS Yasar Ozyigit



MICROBIOLOGIC TECHNOLOGY FOR PURIFYING COASTAL AQUACULTURE WATER Yalu Shao, Hua Zhong, Lihua Chen	3796
STUDY ON TREATING ANTIBIOTIC PRODUCTION WASTEWATER VIA ADVANCED OXIDATION PROCESS (AOP) ${f Li}$	3803
DETERMINATION OF TEMPERATURE INCREASE AND LETTUCE <i>(LACTUCA SATIVA L. DUNA)</i> YIELD IN LOW TUNNELS WITH DIFFERENT PLASTIC COVER MATERIALS INSTALLED IN HIGH-TUNNEL Hasan Oz, Atilgan Atilgan	3807
THE EFFECT OF MAGNETIC FIELD APPLICATIONS TO CHEMICAL CONTENT OF STRATIFIED AND UNSTRATIFIED SEEDS OF SYCAMORE MAPLE ( <i>ACER PSEUDOPLATANUS</i> L.) Sezgin Ayan, Burcu Hasdemir, Nezahat Turfan, Halil Baris Ozel, Esra Nurten Yer	3815
effects of triflumuron on larval intugement of sixth-instar <i>galleria mellonella</i> (l.) (lepidoptera: pyralidae) <b>Sadettin Unsal, Naci Gorer</b>	3823
EFFECT OF GROWTH CHARACTERISTICS ON CONE AND SEED PRODUCTION IN TAURUS CEDAR ( <i>CEDRUS LIBANI</i> A. RICH.) Yilmaz Catal, Nebi Bilir, Halil Baris Ozel	3832
RESPONSE OF SOIL ENZYMES TO TWO ANTIBIOTICS: POLYMYXIN B AND PENICILLIN G Arkadiusz Telesinski, Maciej Platkowski, Krystyna Cybulska, Natalia Telesinska, Jacek Wrobel, Barbara Pawlowska	3837
EFFECT OF REDUCED AND INCREASED HERBICIDES DOSES ON WEED CONTROL STRATEGIES IN CHICKPEA ( <i>CICER ARIETINUM</i> L.) Muharrem Kaya, Aykut Sener, Ruziye Karaman, Mehmet Atak, Asuman Kan	3846
URBAN PEOPLE'S PERCEPTIONS OF ORGANIC PRODUCTS AND THEIR ATTITUDES: AN EXAMPLE FROM TURKEY ${f Sevinc Basay}$	3854
<b>ERRATUM</b> ULTRASOUND-ASSISTED MODIFICATION OF FLAX WASTES TO REMOVE METHYL VIOLET FROM AQUEOUS SOLUTION <b>Xuanxuan Dan, Xiaomin Li</b>	3863



# LALA CLAM (ORBICULARIA ORBICULATA) SHELL AS AN ADSORBENT FOR ANIONIC AND CATIONIC DYES FROM AQUEOUS SOLUTION

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#### ABSTRACT

In this work, lala clam shell was utilised as an alternative low-cost adsorbent for the remediation of water contaminated by two classes of dyes, namely anionic (Congo red (CR) and Methyl orange (MO)) and cationic (Methylene blue (MB) and Rhodamine B (RB)) dyes from aqueous solution. Batch adsorption experiments were performed to assess the effects of various experimental parameters such as solution pH, adsorbent dosage and initial adsorbate concentration. The applicability of lala clam shell to remove dyes from aqueous solution was evaluated in both single- and mix-systems. The optimum pH for CR, MO and RB removal was found at pH 2.0, while pH 8.0 was the optimum value for MB adsorption. At an initial concentration of 2.5 to 100 mg/L, the amount of four dyes adsorbed onto lala clam shell was in the order of CR> MB> RB> MO, in a singledye adsorption system. Whereas, in the case of a mix-dye adsorption system, the amount of four dyes adsorbed was found in the order MB> RB> MO> CR. The adsorption equilibrium data were correlated with both Langmuir and Freundlich isotherm models. The results showed that the equilibrium data were perfectly represented by the Freundlich isotherm model. The biomass adsorbent was characterised using the Field Emission Scanning Electron Microscope (FESEM) and Fourier Transform Infrared (FTIR) Spectrometer. Overall, outcomes from this study suggested that lala clam shell, a fishery waste, can be beneficial and efficient instead of expensive adsorbents for water treatment.

#### **KEYWORDS:**

Adsorption, lala clam shell, dyes, water treatment

### **INTRODUCTION**

Water contamination by various pollutants such as dyes, heavy metals and pesticides poses a serious threat to the environment and human health. Both organic and inorganic substances with a nonbiodegradable characteristic can be accumulated in the environment. Water contamination causes around five million of the world population to die every year [1, 2]. Many industrial activities particularly plastic, textile, printing, transportation, food and leather [3, 4] have significantly contributed to water contamination. As a matter of fact, about 15% of dye contaminations are derived from textile and other industries, worldwide [5, 6]. For example, it was estimated that about 950 million tonnes of dyeing wastewater were produced in China in 2012 [7]. Hence, the treatment of water from these polluted environments is important for the ecological protection [8].

Dyes are classified based on their nuclear structure, namely as anionic and cationic. Anionic dyes have a negative charge due to the presence of sulphonate groups, meanwhile cationic dyes have a positive charge due the presence of protonated amine or sulphur groups in the aqueous solution. Industrial effluents containing both anionic and cationic dyes are of great concern. The anionic dyes (Congo red and Methyl orange) and cationic dyes (Methylene blue and Rhodamine B) are toxic and even carcinogenic [9]. Toxic dyes are normally presence in water environment at high concentrations. Due to their thermal stability as well as ability to absorb and reflect sunlight that enters the water, the photosynthesis of algae and aquatic plants will be reduced. This scenario will seriously affect the food chain. Furthermore, the presence of little amount of dyes in water can be highly visible and undesirable, making it unsafe for the human consumption [10]. For example, excessive levels of Methylene blue may cause a number of diseases such as digestive and respiratory systems problems, as well as nausea, vomiting and profuse sweating [11].

Chemical precipitation, coagulation-flocculation, electrochemical treatment and adsorption have been employed to sequester dyes from aqueous solution [12, 13]. Adsorption is one of the most effective treatment processes as it is a simple operation and incurs low operational cost as compared to other techniques; which have drawbacks like sludge formation, high energy and conservation cost. Undoubtedly, activated carbon is a popular and widely used adsorbent for organic dyes removal. This is



mainly due to its large surface area and high adsorption capacity. However, its application in developing countries is limited due to its high-cost production and regeneration issue [14, 15]. In 2013, the global market for activated carbon totalled \$1.9 billion, driven primarily by Asia-Pacific and North American regions for application in water treatment and then reached \$2.1 billion, in 2014 [16].

Effective adsorbents for water treatment should have several characteristics such as low-cost, readily available in large quantities and easily can be disposed. The capability of several low-cost and ecofriendly adsorbents such as *Luffa cylindrica* biomass [8], *Metroxylon* spp. waste [17], rice straw [11], orange peel [18], mesoporous hollow shells [5] and *Raphia hookerie* epicarp [3] to treat dye contaminated water has been assessed in the last few years. The key property was the presence of functional groups (hydroxyl, amine and carbonate) and lignocellulosic compounds in these adsorbents that contributed to bind dyes during the adsorption process.

In the present work, the natural waste from fishery industry, namely the short neck clam (Orbicularia orbiculata) shell or locally known as lala was used as an alternative adsorbent for water treatment. Lala clam shell is abundantly available in Malaysia, Indonesia and Libya with no economic value. It has not been used for purification of water contaminated by dyes. Moreover, the shell waste is primarily composed of calcium carbonate (95%), which may be beneficial for the adsorption mechanism [19]. Hence, the main objective of this study was to investigate the effectiveness of lala clam shell as an adsorbent for the removal of anionic and cationic dyes from aqueous solution in the single- and mix-dye systems. A systematic evaluation involving several experimental parameters such as the pH solution, initial adsorbate concentration and adsorbent dosage was performed.

#### **MATERIALS AND METHODS**

**Chemicals.** Lala clam shells were collected from a restaurant in Tanjong Malim, Perak. NaOH and HCl were purchased from HmbG Reagent Chemicals. In this work, two anionic (CR and MO) and two cationic (MB and RB) dyes were studied. The chemical structure and physiochemical properties of dyes studied are listed in Table 1. CR, MB and RB were supplied by Merck, while MO was acquired from Bendosen. All chemicals used were of analytical grade and deionised water was used throughout this study.

**Preparation of adsorbent and adsorbate.** The lala clam shells were washed and rinsed by using tap water, then thoroughly with deionised water to remove dirt. Finally, the shells were dried in an oven at 70 °C for 24 h. After drying, the shells were crushed and sieved through 150-250  $\mu$ m size fractions by using a protocol of the American Society for Testing and Materials (ASTM) standard sieve. The stock solutions of 100 mg/L were prepared with appropriate amount of dyes (CR, MO, MB and RB) by dissolving in the deionised water. Each dye was prepared separately by dissolving 25 mg of the dye in 250 mL deionised water and then, the stock solution was diluted to the required concentrations.

**Characterisation studies.** The surface area and average pore diameter analyses were performed using a Quantachrome Autosorb 1 Surface Analyser. The Brunauer-Emmett-Teller (BET) multipoint technique [20] was applied for surface area measurement, while the Barrett, Joyner and Halenda method [21] was used for pore diameter determination.

The presence of functional groups on materials, as well as the interaction between functional groups with dyes were identified and studied using a Thermo Nicolet 6700 Fourier Transform Infrared (FTIR) Spectrometer. FTIR analysis was conducted over 32 cumulative scans in the wavenumber ranging from 4000 to 400 cm<sup>-1</sup>. The surface morphology of the Lala clam shells before and after dye adsorption was examined using a Hitachi SU 8020 UHR Field Emission Scanning Electron Microscope (FESEM).

Adsorption experiments. The batch adsorption experiments were carried out in 250 mL conical flasks by adding approximately 0.5 g of an adsorbent in 50 mL of dye solution of the desired concentration at optimum conditions. The samples were equilibrated by shaking at 100 rpm for 1 h using a Protech Orbital Shaker (model 720) and samples were separated through a piece of filter paper (Filtre Fioroni 601, 110 mm). The concentration of dyes was measured using an Agilent Cary 60 UV-Vis spectrophotometer at maximum wavelength ( $\lambda_{max}$ ) values as shown in Table 1. The calibration curve was lined between the absorbance and various concentration of the dye solution (1, 2, 3, 4 and 5 mg/L) to acquire the absorbance-concentration profile (equilibrium dye concentration).

The effect of pH solution was studied in the pH range of 2.0-8.0. The pH solution was adjusted by adding a few drops of diluted 0.05 mol/L HCl or 0.05 mol/L NaOH solutions, and measured using a pH meter. About 0.5 g of the adsorbent was added to 50 mL of 5 mg/L dye solution. The mixture was then shaken for 1 h at 100 rpm. The isotherm studies were accomplished by shaking 0.5 g of adsorbent in 50 mL of dye solution with an initial dye concentration ranging from 2.5 mg/L to 100 mg/L. The experiment was performed at an optimum pH. The effect of adsorbent dosage on adsorption capacity was studied using four various doses of adsorbent, ranging from 0.025 g to 0.200 g. The adsorbent was added into 50



mL of 5 mg/L dye solution, shaken and filtered as described earlier.

The competitive adsorption study was accomplished in the mix-dye system. About 0.5 g of lala clam shells was added to 50 mL solution containing (5, 20 or 100 mg/L) of each dye. The adsorption of the mix-dye system was investigated using a similar procedure to that of the single-dye system experiment. The equilibrium concentration of each dye was measured using the UV-Vis spectrophotometer. The dried filtrate was characterised using FTIR and FESEM.

All experiments were run in triplicates. The adsorption capacity at equilibrium (q) was calculated using Equation (1):

$$q = \frac{\left(C_o - C_e\right)}{W}V\tag{1}$$

where q is the amount of dye adsorbed at equilibrium (mg/g),  $C_0$  is the initial dye concentration (mg/L),  $C_e$  is the equilibrium dye concentration (mg/L), W is the weight of the adsorbent (g) and V is the volume of dye solution (L). The removal percentage of dye for the adsorption process was estimated using Equation (2):

Removal % = 
$$\frac{\left(C_{o} - C_{e}\right)}{C_{o}} \times 100$$
 (2)

Dyes	Chemical structures	Molecular weight (g/mol)	$\lambda_{max}$ (nm)	Industrial use
Congo Red (CR)	$\begin{array}{c} 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $	696.67	499	Textiles, paper and rubber.
Methyl Orange (MO)	$H_3C$ $N$	327.34	461	Printing and research laboratories.
Methylene Blue (MB)	H <sub>3</sub> C N CH <sub>3</sub>	319.85	665	Wood, silk and cotton.
Rhodamine B (RB)	CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub> CH <sub>3</sub>	479.02	554	Textiles, paper and leathers.

 TABLE 1

 The chemical structure and physiochemical properties of dyes studied.





Effect of solution pH on adsorption of anionic dyes (a) and cationic dyes (b) onto lala clam shell.

### **RESULTS AND DISCUSSION**

Adsorption studies. Single-dye system. Effect of solution pH. The expulsion of dyes from wastewater by adsorption is highly reliant on the pH of the solution, which influences the surface charge of the adsorbent, degree of ionisation and speciation of the adsorbate [22].

Figures 1(a) and 1(b) show the effect of pH solution on the percentage removal of anionic and cationic dyes by lala clam shells, respectively. It was clear that the percentage removal of two anionic dyes (CR and MO) decreased with an increase in the pH and optimum pH was recorded at pH 2.0 (Figure 1(a)). A similar optimum pH value was observed for adsorption of CR onto biomass of *Trametes pubescens* [23], adsorption of MO onto chitosan [24] and activated carbon [25]. This observation can be related to electrostatic repulsion between the sulfonates (SO<sub>3</sub><sup>2-</sup>) groups and excessive OH<sup>-</sup>ions at the high pH values.

In contrast, the effect of pH solution on the percentage removal of two cationic dyes (MB and RB) by lala clam shells is shown in Figure 1(b). The percentage removal of MB increased with an increase in the pH and the maximum removal efficiency was achieved at pH 8.0. In this case, the percentage removal of RB was decreased with an increase in the pH and the maximum efficiency was obtained at pH 2.0. A similar trend was reported for adsorption of MB by tea waste [26], *Imperata cylindrical* biomass [27] and adsorption of RB by steel slag [28]. The adsorption behaviour of MB and RB was greatly influenced by their functional groups.

MB, like other cationic dyes produced an intense molecular cation ( $C^+$ ) and reduced ions ( $CH^+$ ), which exists in aqueous solution in the form of positively charged ions [29, 30]. Thereby, the high pH values will cause the adsorbent surface become negatively charged and results in higher adsorption. Meanwhile, RB contains a carboxyl group structure as shown in Table 1. The sharp decreased in percentage removal at the higher pH values was likely due to electrostatic repulsion between the carboxyl group and the excessive hydroxide ions.

Effect of adsorbent dosage. The adsorbent dosage is one of the important parameters in determining the capacity of adsorbent and fundamental to optimise an adsorption system as adsorbent dosage controls the availability of adsorption site [31, 32]. Figure 2 presents the effect of adsorbent dosage on adsorption of CR, MB, RB and MO onto lala clam shells. It was observed that as the amount of adsorbent was increased, a sharp decrease in adsorption capacity from 9.8 mg/g to 1.5 mg/g, 7.5 mg/g to 0.8 mg/g, 1.5 mg/g to 0.2 mg/g and 2.5 mg/g to 0.1 mg/g was obtained for CR, MB, RB and MO, respectively.

A lower adsorbent dosage which presumed a larger overall total surface area of lala clam shell was being exposed and thus more dyes were adsorbed onto the surface per gram unit of lala. Besides, the higher adsorbent dosage surface of lala clam shell became masked due to the accumulation particles on the adsorbent; it thus created adsorbent aggregation and reduction in the total surface area of contact by the active sites, namely carbonate group ( $CO_3^{2-}$ ) of lala clam shell. The same behaviour of other adsorbents on dyes was reported in the literature [22, 33, 34, 35].

Effect of initial adsorbate concentration. Experiments were carried out at different initial concentrations (2.5 to 100 mg/L) of dye, while the other parameters were kept constant and performed at optimum pH. Figure 3, presents the amount of dye ad-



sorbed as a function of initial concentration. It is essential to note that the amount of all dyes adsorbed by lala clam shells increased with an increase in the initial concentration of the dye solution. This outcome can be explained by two main factors, namely: (1) the probability of the increase due to the collision between the molecules of dyes and adsorbent surface, and (2) the high diffusion rate of dyes into adsorbent [36].

The amount of four dyes adsorbed onto lala clam shells was in the order of CR > MB > RB >MO. Although CR is an anionic dye, it contains two amine groups (-NH<sub>2</sub>) and diazo groups (-N=N-) that can be potential protonation sites, and thus there are different possible types of protonated dye molecules [37]. Figure 4 shows the protonated CR at optimum pH [37, 38].

From Figure 4, in the acidic condition at optimum pH 2.0, it can be imagined that the protonated amino (NH<sub>3</sub><sup>+</sup>) or azo nitrogens (-N=NH<sup>+</sup>) having positive charge can be adsorbed over the high negatively charged  $CO_3^{2-}$  surface of lala clam shells. However, MO is also an anionic dye but contains one azo group (-N=N-), so it comes last in the order after two cationic dyes that can be adsorbed more than MO onto the surface of lala clam shells.



FIGURE 2 Effect of adsorbent dosage on adsorption of MB, RB, CR and MO.



Effect of initial concentration on adsorption of MB, RB, CR and MO.





FIGURE 4 Protonated of CR at optimum pH 2.0. Adapted from [37, 38].

 TABLE 2

 Freundlich and Langmuir isotherm constants for adsorption of CR, MO, MB and RB onto lala clam shells.

Duas		Freundlich			Langmuir	
Dyes	$K_{\rm F} ({\rm mg/g})$	1/n	$R^2$	$Q_{\rm max} \ ({\rm mg/g})$	b (L/mg)	$R^2$
CR	4.375	0.726	0.962	15.480	0.559	0.739
MO	0.010	0.677	0.959	1.004	0.013	0.286
MB	0.320	0.825	0.998	11.669	0.028	0.609
RB	0.014	0.496	0.699	0.311	0.047	0.641

Adsorption isotherms. The interaction and distribution of dyes on the surface of adsorbent are described using the adsorption isotherm models [36, 14]. Two widely used isotherm models, namely Freundlich and Langmuir were applied to analyse equilibrium data. Freundlich isotherm model is an empirical equation used to describe adsorption at multilayer heterogeneous with sites that had different energies of adsorption [14]. The linear form of the Freundlich equation is expressed as Equation (3) [39].

$$\log q_{\rm e} = \log K_{\rm F} + \frac{1}{n} \log C_{\rm e} \tag{3}$$

where  $C_e$  is the equilibrium concentration of solute (mg/L),  $q_e$  the amount of solute adsorbed per unit weight of adsorbed at equilibrium (mg/g),  $K_F$  (mg/g) and n are the Freundlich constants related to adsorption capacity and intensity, respectively. The liner plot of log  $q_e$  against log  $C_e$  will give the  $K_F$  and n values.

The Langmuir isotherm model deals with adsorption at monolayer homogeneous surface of the adsorbent where all sites on adsorbents have equal energy [36]. The linear form of the Langmuir isotherm is represented by Equation (4) [40].

$$\frac{C_{\rm e}}{q_{\rm e}} = \frac{C_{\rm e}}{Q} + \frac{1}{Qb} \tag{4}$$

where Q is the maximum adsorption at monolayer (mg/g) and b is the Langmuir constant related to the affinity of binding sites (mL/mg). In addition, b is a measure of the energy of adsorption. The Q and b can be determined from the linear plot of  $C_e/q_e$  against  $C_e$ .

The isotherm constants and correlation coefficient ( $R^2$ ) obtained from Freundlich and Langmuir isotherm models are listed in Table 2. Based on  $R^2$ values, the equilibrium adsorption data for all dyes fitted the Freundlich isotherm model better than Langmuir isotherm, indicating the heterogeneous of the adsorbent surface. Similar results were obtained by Dey et al. [36] for MB removal using *Rhizopus oryzae* waste, Mahmoud et al. [18] for CR and MO adsorption using orange peel, and Balasubramani and Sivarajasekar [41] for RB removal using activated carbon. The 1/n values calculated from the Freundlich isotherm model lie between 0 and 1. This implies that the adsorption of four dyes onto Lala clam shells was favourable [42].

The adsorption capacities  $K_{\rm F}$  calculated from the Freundlich isotherm equation for CR, MO, MB and RB, were 4.375, 0.010, 0.320 and 0.010 mg/g,



respectively. The removal of dyes by using several other adsorbents has been studied in the recent years and some of these reports provided  $K_{\rm F}$  values. Although these values were obtained under different experimental conditions, they were useful to compare the performance and capacity of the adsorbents. The K<sub>F</sub> value obtained in this study was greater than those reported for kaolin (1.089 mg/g for CR) [43], aminefunctionalized hollow mesoporous shells (1.291 mg/g for CR) [5], Rhizopus oryzae (0.021 mg/g for MB) [36], sugarcane bagasse (0.110 mg/g for MB) [31] and activated geopolymer (0.002 mg/g for MO) [44].

The essential characteristics of the Langmuir isotherm can be expressed by a separation factor  $(R_{\rm L})$ , which is defined in the following Equation (5) [42]:

$$R_{\rm L} = \frac{1}{1 + bC_{\rm c}} \tag{5}$$

where  $C_0$  is the initial adsorbate concentration (mg/L),  $R_L$  is the value shows the nature of the adsorption process to be unfavourable  $(R_L>1)$ , linear  $(R_{\rm L} = 1)$ , favourable  $(0 < R_{\rm L} < 1)$ , or irreversible  $(R_{\rm L} =$ 0). The R<sub>L</sub> values were 0.187, 0.825, 0.718 and 0.634 for CR, MO, MB and RB, following the adsorption by lala clam shells. It is clear that the  $R_L$  values were in the range of  $0 < R_L < 1$ . This suggests that the adsorption of four dyes was favourable.

The maximum adsorption capacity Q (mg/g) of lala clam shells for CR, MO, MB and RB were 15.48, 1.00, 11.66 and 0.31 mg/g, respectively. It was compared to other adsorbents. The maximum adsorption capacities of lala clam shells were compared to several other adsorbents, as shown in Table 3. The difference in Q values of the adsorbents can be related to their unique physical and chemical characteristics [54] and experimental conditions.

TABLE 3
The maximum adsorption capacities ( $O_{max}$ ) of several adsorbents.

The maximum ausor prior capacities (Qmax) of several ausor bents.					
Adsorbents	Dye	$Q_{\rm max}({ m mg/g})$	References		
Eichhornia crassipes root	CR	1.58	[45]		
Peanut shell	CR	15.09	[46]		
Zeolite	CR	3.77	[47]		
Calcareous soil	MB	1.76	[33]		
Cow dung ash	MB	5.31	[48]		
Luffa cylindrical	MB	4.94	[8]		
Rhizopus oryzae biomass	MB	8.20	[36]		
Rice husk ash	MB	6.90	[49]		
Spent rice biomass	MB	8.30	[50]		
Activated carbon modified by silver nanoparticles	MO	0.69	[51]		
Fly ash	MO	1.20	[52]		
Humicola fuscoatra biomass	MO	0.50	[53]		

Adagemention quatern	Driag	Dye con	Amount of dye	
Ausorption system	Dyes	Initial	Equilibrium	adsorbed (mg/g)
		5	0.57	0.44
	MB	20	3.64	1.64
		100	4.32	9.56
		5	3.00	0.22
	RB	20	10.55	0.95
Single-dye		100	13.01	8.73
system		5	3.99	0.10
	MO	20	15.06	0.49
		100	57.30	4.28
		5	0.10	0.48
	CR	20	0.32	1.96
		100	1.59	9.84
		5	0.67	0.43
	MB	20	1.51	1.84
		100	2.02	9.78
		5	2.86	0.21
	RB	20	10.32	0.96
Mix-dye system		100	12.33	8.75
		5	4.21	0.07
	MO	20	14.31	0.56
		100	57.23	4.27
		5	4.72	0.02
	CR	20	18.95	0.10

TABLE /

59.13

4.08

100



A de entreut	Duna	Dyes conc	Dyes concentration (mg/L)		
Adsorbent	Dyes	Initial	Equilibrium	dyes (mg/g)	
		5	0.67	0.43	
	MB	20	1.51	1.84	
		100	2.02	9.78	
		5	2.86	0.21	
	RB	20	10.32	0.96	
Lala clam		100	12.33	8.75	
shell		5	4.21	0.07	
	MO	20	14.31	0.56	
		100	57.23	4.27	
		5	4.72	0.02	
	CR	20	18.95	0.10	
		100	59.13	4.08	
		5	0.54	0.44	
	MB	20	1.50	1.84	
		100	2.70	9.70	
		5	2.06	0.29	
Activated carbon	RB	20	10.54	0.94	
darived from		100	15.44	8.44	
mengrova stam		5	4.96	0.01	
mangrove stem	MO	20	15.28	0.47	
		100	61.52	3.84	
		5	4.91	0.01	
	CR	20	19.29	0.07	
		100	64.81	3.51	

TABLE 5

Comparison of amount of dyes adsorbed onto lala clam shell and activated carbon in mix-dye system.

Adsorption studies. Mix-dye system. It is important to study the potential of lala clam shells to adsorb dyes in the mix-dye system because of their general existence in real water and wastewater. In this study, four dyes were mixed at different initial concentrations of 5, 20 and 100 mg/L. All experiments were performed with 0.5 g of lala clam shells. Table 4 shows the amount of MB, RB, MO and CR adsorbed onto lala clam shells at different initial dye concentration of 5, 20 and 100 mg/L.

It was noticed that the amount of MB, RB and MO adsorbed were convergent somewhat in both the single and mix-dye systems at different initial concentration of 5, 20 and 100 mg/L. A different amount of adsorption was observed for CR. The amount of CR adsorbed by lala clam shells decreased from 0.48, 1.92 and 9.75 mg/g (single-dye system) to 0.02, 0.08 and 3.90 mg/g (mix-dye system) at initial concentration of 5, 20 and 100 mg/L, respectively. The ability of lala clam shells to adsorb dyes in the mix-dye system was in the order of MB > RB > MO > CR, meanwhile a different trend was obtained for single-dye system of which the order was CR > MB > RB > MO.

It was observed that the amount of CR adsorbed became last in the order of the mix-dye system. This can be explained by two main factors: (1) for mixdye system, the experiment was not performed at the optimum pH value of each dye, which purposely to mimic real wastewater environment, and (2) CR is an anionic dye that possess a negative charge and larger size as compared to MO. In contrast, MB is the cationic dye that has a positive charge and smaller size than RB, which might lead to a stronger affinity with the negatively charge of lala clam shells. The impacts of the competing ions observed in the present study are also relevant to the earlier reports [55-57].

Besides, Table 5 shows the comparison of the amount of dyes adsorbed by lala clam shells and activated carbon derived from mangrove stem in the mix-system. From Table 5, it was clear that MB was the best dye adsorbed by both adsorbents in the mixsystem, in the order of MB > RB > MO > CR. The results suggest that lala clam shells have a good potential and can replace activated carbon to remove dyes from wastewater. For example, with 100 mg/L of initial concentration of dyes at the equilibrium, the concentration was decreased to 2.02, 12.33, 57.23 and 59.13 mg/L for MB, RB, MO and CR, respectively. It was observed that the equilibrium concentration became less than 50% for cationic dyes and about 50% for anionic dyes following treatment with lala clam shells, indicates a great potential for future applications.

Characterisation studies. Surface area and pore diameter. The surface area, pore volume and pore diameter of lala clam shells were measured as  $2.09 \text{ m}^2/\text{g}$ ,  $0.164 \text{ cm}^3/\text{g}$  and 0.147 nm, respectively. According to the International Union of Pure and Applied Chemistry (IUPAC) classification, the pore of the lala clam shells is considered as micropores (d < 2 nm).

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FTIR analysis. FTIR is an effective analytical instrument for identifying functional groups and characterising covalent bonding information. The FTIR spectra of the lala clam shells, before and after the adsorption of dyes are shown in Figure 5. Based on Figure 5, the two prominent bands appeared at 1448 cm<sup>-1</sup> and 853 cm<sup>-1</sup> are the characteristics of carbonate ( $CO_3^{2-}$ ) [58]. The band at 1781 cm<sup>-1</sup> can be assigned to carbonyl (C=O) groups. There were significant changes in the FTIR spectrum of lala clam shells after interaction with dyes. For example, the absorption band of CO32- group at 1448 cm<sup>-1</sup> shifted to 1444, 1464, 1462 and 1467 cm<sup>-1</sup> following the interaction with CR, MO, MB and RB. In addition, the absorption intensity of this band decreased after the adsorption of MB. Presumably, the shift in wavenumber of the functional groups may be due to the interaction of dyes with active sites of the adsorbent [59]. A new peak observed at 2630 cm<sup>-1</sup> after interaction with MO can be assigned to C-H stretching. Overall, it is evident from FTIR analysis that carbonate group is the main adsorption site in lala clam shells.

FESEM analysis. FESEM analysis was performed to observe the surface morphology of the lala clam shells before and after the interaction with dyes. The analysis is also useful for determining the particle shape. The FESEM images of lala clam shells before and after being loaded with CR, MO, MB and RB at 10,000x magnifications are shown in Figures 6. Lala clam shells have an uneven structure with non-uniform size distribution on the surface (Figure 6(a)). Subsequent interaction with dyes, the surface of lala clam shells became rough, more uneven and heterogeneous (Figures 6(b), 6(c), 6(d) and 6(e)). The change in the surface morphology of lala clam shells could be due to the reorganisation of surface functional groups binding the CR, MO, MB and RB molecules [60]. From Figure 6(d), it is clear that lala clam shells are covered by MB molecules adsorbed. A similar observation was reported by Su et al. [27] for adsorption of MB onto Imperata cylindrica (Cogon grass).



FIGURE 5 The FTIR spectra of lala clam shell (a) before and after adsorption of (b) CR, (c) MO, (d) MB and (e) RB.





FESEM images of lala clam shell before dye adsorption (a) and after adsorption of CR (b), MO (c), MB (d) and RB (e) at 10, 000× magnification.

## CONCLUSIONS

As elucidated throughout the study, lala clam shells have several significant advantages over established adsorbents for water treatment. Most notably advantages are abundant availability and good performance, which can be used as an alternative low-cost adsorbent for the removal of dyes from aqueous solution. Its key property is the presence of carbonate group ( $CO_3^{2-}$ ) that can bind functional groups of dyes during the adsorption process. The adsorption process is greatly influenced by several experimental parameters such as the pH solution, initial dye concentration and adsorbent dosage. The order of selective adsorptions was different in the single- or mix-dye system. The equilibrium data fitted very well with the Freundlich isotherm equation. The adsorption performance of lala clam shells was comparable with mangrove stem derived activated carbon, a commercial adsorbent used in water treatment. Therefore, the developed adsorption treatment system is useful and applicable for the removal of organic dyes from contaminated water.

## ACKNOWLEDGEMENTS

The authors would like to Miss Siti Najiah Mohd Yusoff, Mrs. Johana Jumiran, Mr. Mohd Zurin Mahmood, Mr. Ibrahim Saidin and Mr. Hashimi Ma'ani for their technical assistance.

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<b>Received:</b>	19.10.2017
Accepted:	13.03.2018

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